

# THE IV BALTIC BIOGAS FORUM

Efficiency of sulphur compounds removal - long-term  
studies of system applying modified mineral sorbent

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## Chemical composition of biogas obtained from different kind raw materials

Component	Unit	Biogas from OFMSW	Biogas from WWTP	Agricultural biogas	Biogas from agricultural and food wastes
Methane	[% ]	50 - 60	60 - 75	60 - 75	68
Carbon dioxide	[% ]	34 - 38	19 - 33	19 - 33	26
Nitrogen	[% ]	0 - 5	0 - 1	0 - 1	-
Oxygen	[% ]	0 - 1	<0.5	<0.5	-
Water	[% ] (40°C)	6	6	6	6
Hydrogen sulphide	[mg/m <sup>3</sup> ]	100 - 900	1000 - 4000	3000 - 10000	100
Ammonia	[mg/m <sup>3</sup> ]	-	-	50 - 100	400
Aromatic compounds	[mg/m <sup>3</sup> ]	0 - 200	-	-	-
Chlor or fluor organic compounds	[mg/m <sup>3</sup> ]	100 - 800	-	-	-

## Popular sulphur compounds in biogas

Hydrogen sulphide - H<sub>2</sub>S

Sulphides - R<sub>2</sub>S

Disulphides - RSSR

Dimethyl sulphide - CH<sub>3</sub>SCH<sub>3</sub>

Methane thiol - CH<sub>3</sub>SH

Dimethyl disulphid - CH<sub>3</sub>SSCH<sub>3</sub>

Carbon disulphide - CS<sub>2</sub>

Methyltiophene – C<sub>5</sub>H<sub>7</sub>S

Ethyliophene – C<sub>6</sub>H<sub>9</sub>S

Alkyl disulphides C<sub>3</sub> – C<sub>10</sub> : C<sub>3</sub>H<sub>8</sub>S<sub>2</sub> – C<sub>10</sub>H<sub>22</sub>S<sub>2</sub>

Alkyltrisulphide C<sub>6</sub> - C<sub>6</sub>H<sub>14</sub>S<sub>3</sub>

Carbon oxysulphide - COS

Compound	Abbreviation	Molecular weight [g/mol] at 25°C	Water solubility [mg/dm³]	Vapor Pressure at 25°C [kPa]
Trimethyl silanol	-	90	35000	2,13
Hexamethyldisiloxane	L <sub>2</sub>	162	0,93	4,12
Octamethyltrisiloxane	L <sub>3</sub>	236	0,035	0,52
Decamethyltetrasiloxane	L <sub>4</sub>	310	-	0,07
Dodecamethylpentasiloxane	L <sub>5</sub>	384	3,1x10 <sup>-4</sup>	0,009
Hexamethylcyclotrisiloxane	D <sub>3</sub>	222	1,56	1,14
Octamethylcyclotetrasiloxane	D <sub>4</sub>	297	0,056	0,13
Decamethylcyclopentasiloxane	D <sub>5</sub>	371	0,017	0,02
Dodecamethylcyclohexasiloxane	D <sub>6</sub>	445	0,005	0,003



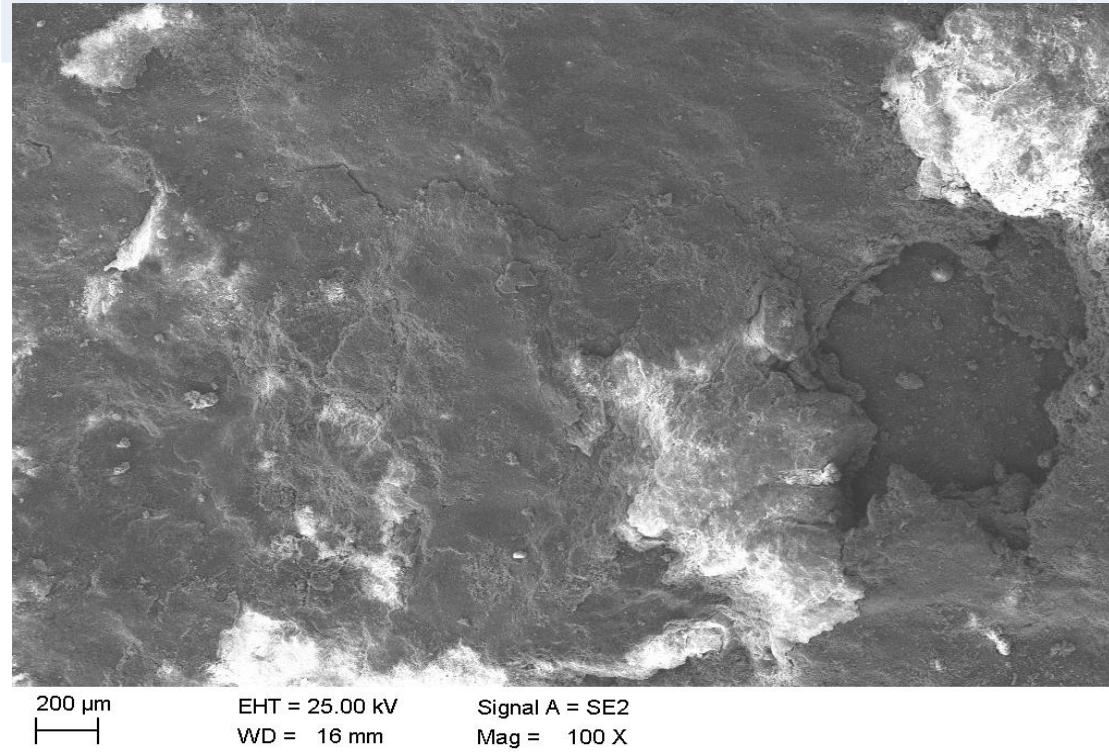
Damaged noise suppressor through sour gasses



View of carbon deposits on cylinders of the engine burning raw biogas after c 1500 working hours.

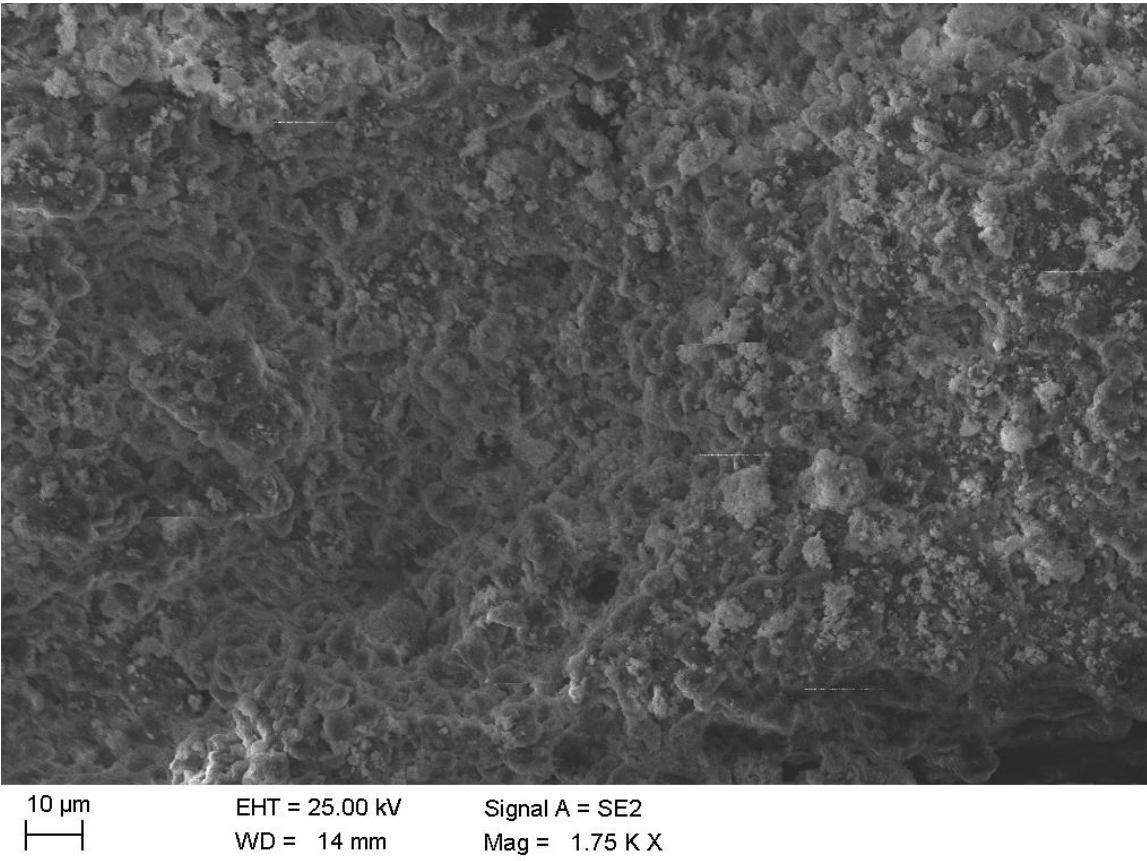
# Results of chemical analyses of the carbon deposit produced in the engine using raw biogas

Elements	Ca	S	Zn	Fe	Na	Si	P	Cu	Al	Mn	Mg
Content [%]	22.2	18.6	10.3	1.6	2.6	3.6	3.1	1.5	1.6	0.6	0.6



Microscopic view SEM of the carbon deposit collected from the head of the engine

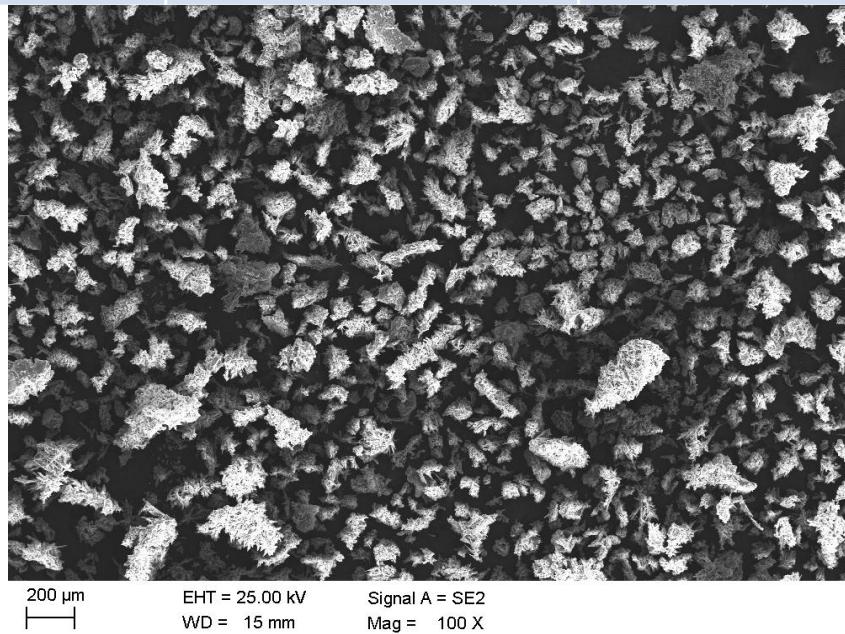
Elements	C	Al	S	Ca	Fe	Na	Zn	P	Si	Ni	Cr
[%]	74.5	3.7	2.2	1.1	0.5	0.4	0.6	0.7	0.2	0.1	0.1



Structure tarry deposit produced on the surface of the heat exchanger

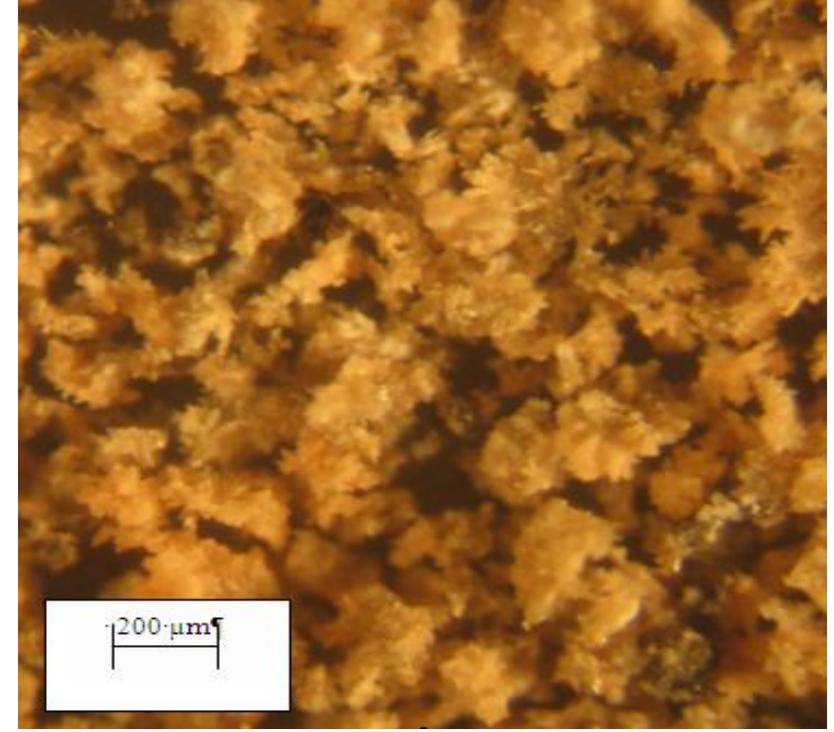
# Results of chemical analyses of deposit accumulated in the filter

Element	Measurement 1	Measurement 2	Measurement 3	Average
O	40,10	39,58	40,71	40,13
Na	24,45	24,32	25,94	24,90
S	27,85	28,26	23,44	26,52
Ca	0,88	1,04	1,78	1,23
Fe	6,71	6,80	8,13	7,21

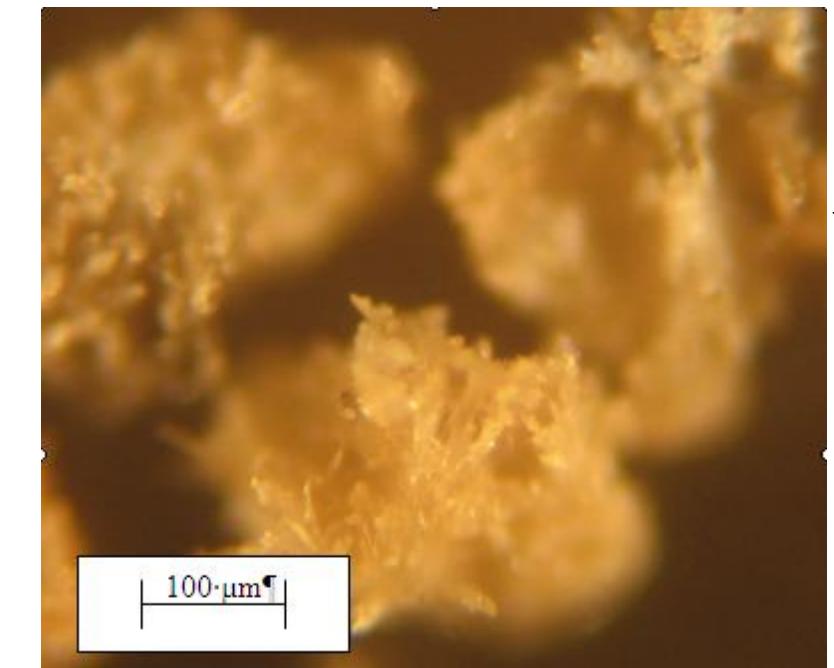


Structure of deposit stored up on the filter

View of deposit in the microscope SEM



View of deposit in the optical microscope





Lp.	Name compound	Designation	Value	Unit
1	Chlorine	Cl	< 100	mg/10 kWh
2	Fluorine	F	< 50	mg/10 kWh
3	Total content of chlorine and fluorine	Sum Cl + F	< 100	mg/10 kWh
4	Dust 3 – 10 µm		< 10	mg/10 kWh
5	Oil		< 250	mg/10 kWh
6	Silicon	Si	< 20	mg/10 kWh
7	Sulphur	S	< 2200	mg/10 kWh
8	Hydrogen sulphide	H <sub>2</sub> S	< 1500	mg/10 kWh
9	Ammonia	NH <sub>3</sub>	< 30	mg/10 kWh
10	Nominal pressure		10	kPa
11	Max. fluctuation of gas pressure		< 0,1	kPa
12	Max. gas temperature		35	°C
13	Max. humidity		80	%

The requirements in relation to the acceptable content of pollutants in biogas

## **Acceptable content of siloxanes**

Internal combustion engines: 5 – 28 mg/m<sup>3</sup>

Gas turbines : < 0,1 mg/m<sup>3</sup>

## **Acceptable content of ammonia NH<sub>3</sub>**

Internal combustion engines: 20 – 50 mg/Nm<sup>3</sup>

## **Acceptable content of H<sub>2</sub>S**

Energy boilers : do 1000 ppm

Internal combustion engines: 50 – 100 ppm

Gas net: 4 – 7 ppm

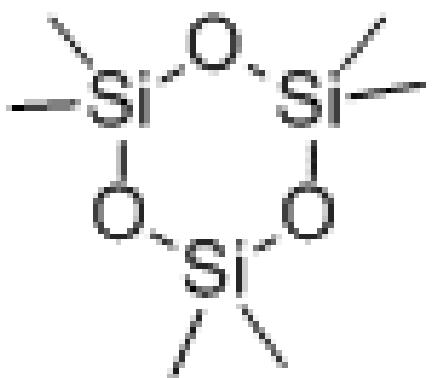
Fuel cells: < 1 ppm

## **Acceptable content of vapour Hg**

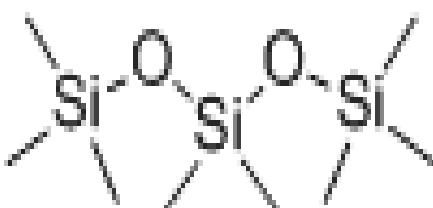
Gas net: 30,0µg/m<sup>3</sup>



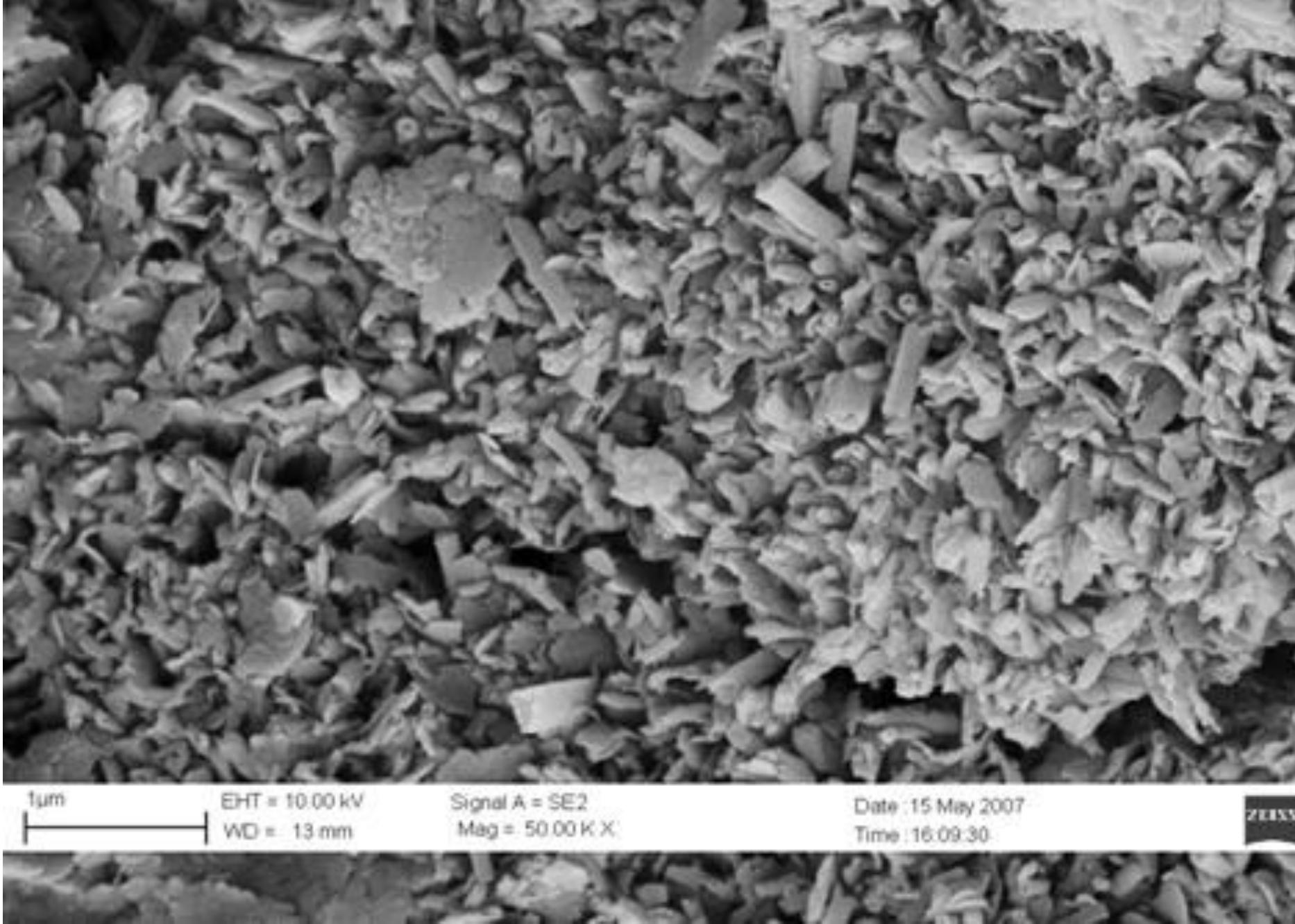
Hexamethyldisiloxane  
 $C_6H_{18}OSi_2$



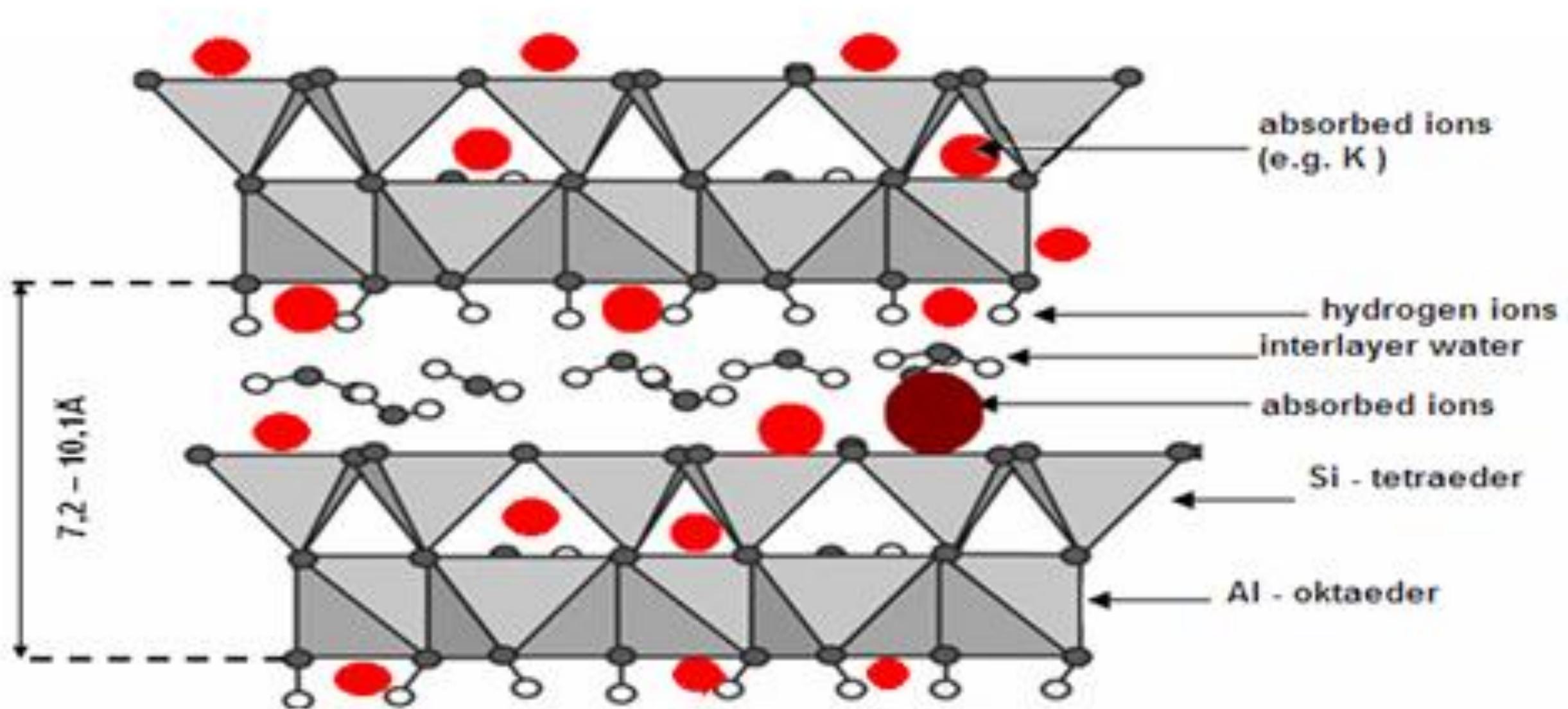
Hexamethylcyclotrisiloxane  
 $C_6H_{18}O_3Si_3$



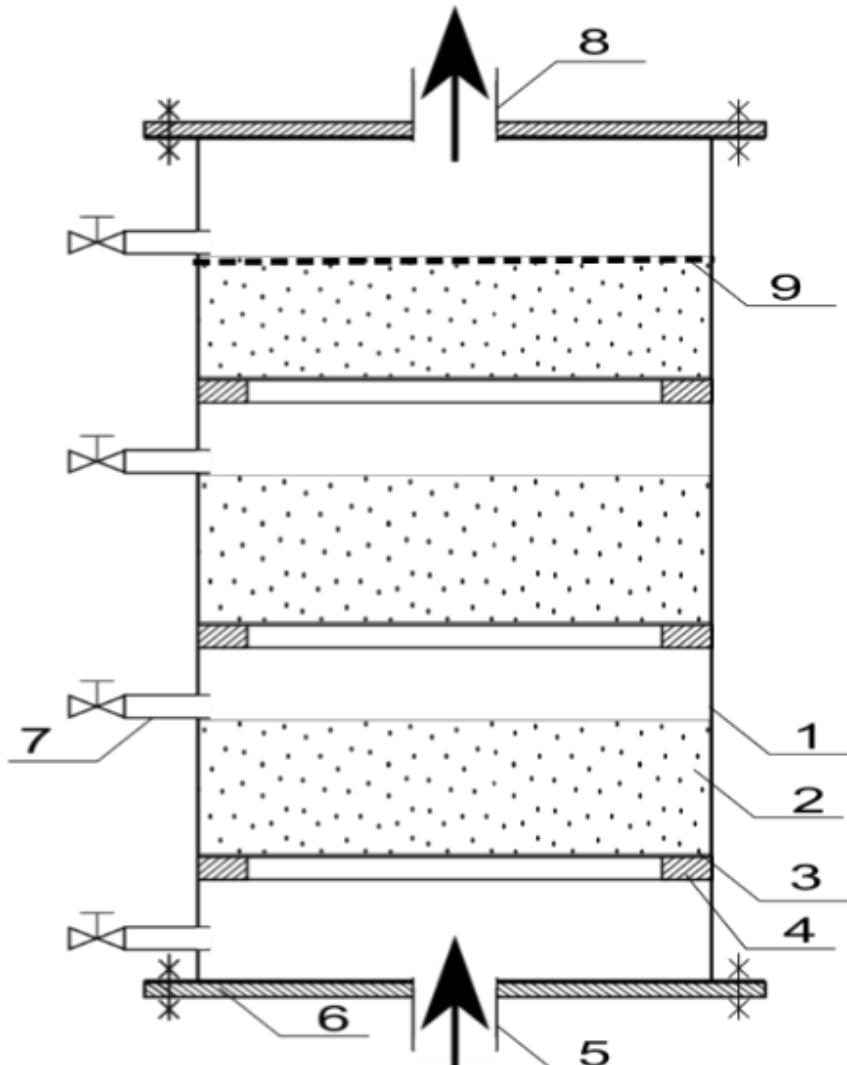
Octamethyltrisiloxane  
 $C_8H_{24}O_2Si_3$



Microscopic view of natural halloisite from the mine Dunino (scale 1  $\mu\text{m}$ )



Layer-cellular structure of halloysite



1 - korpus  
2 - sorbent  
3 - sito  
4 - półka

5 - wlot  
6 - pokrywa  
7 - króciec probierczy  
8 - wylot  
9 - włóknina filtracyjna

# Change of content of the hydrogen sulphide and ammonia after passing biogas by individual layers of the filter

Measurement	Intake	After I shelf	After II shelf	After III shelf	After IV shelf
H <sub>2</sub> S [ppm]	1865	1320	190	20	15
NH <sub>3</sub> [ppm]	2050	1630	1350	960	650
O <sub>2</sub> [%]	0,0	0,0	0,0	0,0	0,0

Measurement	Intake	After I shelf	After IV shelf
H <sub>2</sub> S [ppm]	1955	245	10
NH <sub>3</sub> [ppm]	1990	1250	425
O <sub>2</sub> [%]	0,0	1,6	1,6

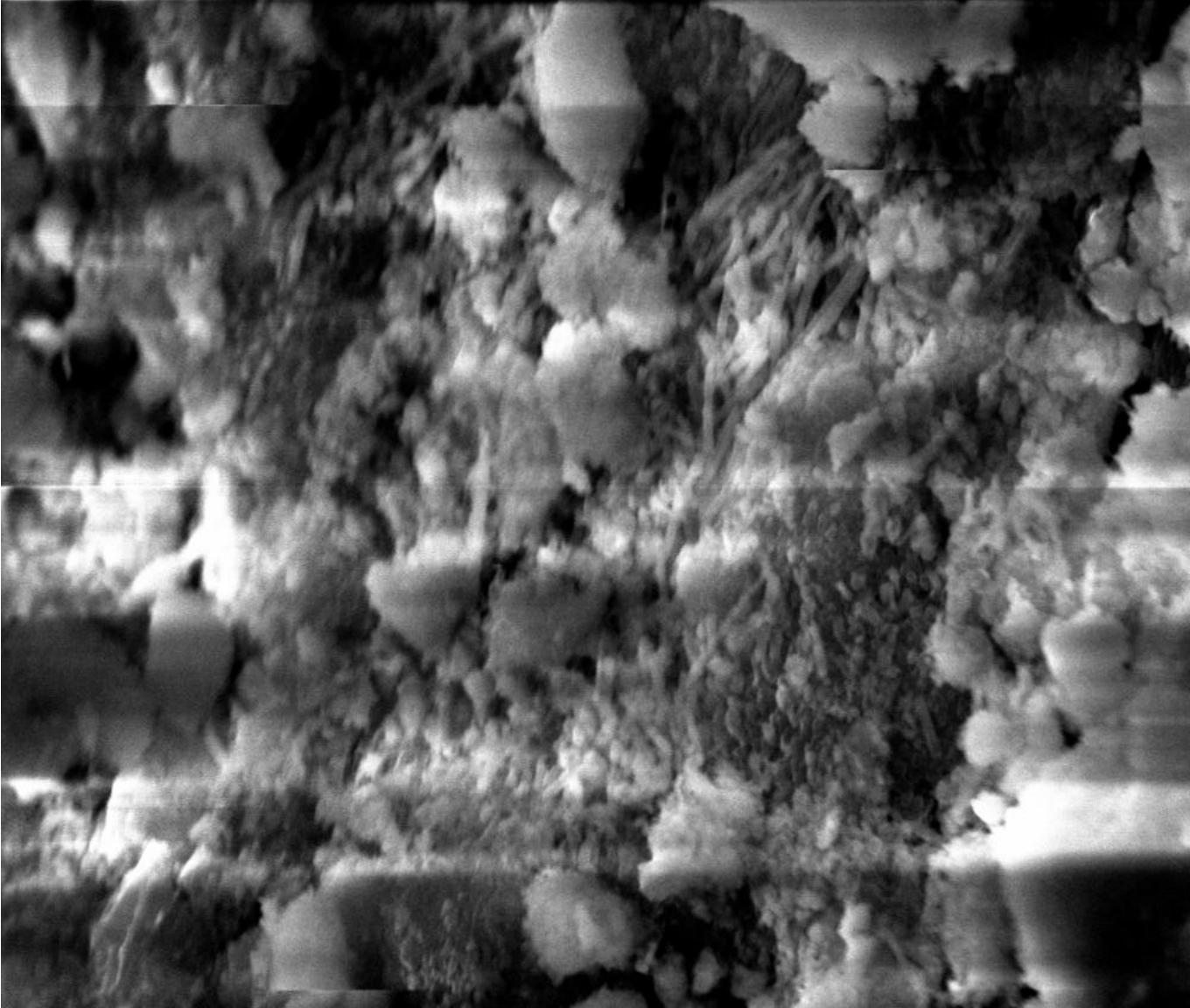
Influence of air addition to the filter

# Changes concentration of the hydrogen sulphide after closing the inflow of air

Time after closing the inflow of air [min]	Concentration of H <sub>2</sub> S [ppm]
0	385
1	600
2	970
3	1215
4	1310
5	1380
10	1360
20	1370



View of sorbent on the IV shelf (outflow). Privileged places of the flow are visible (darker).



2  $\mu$ m

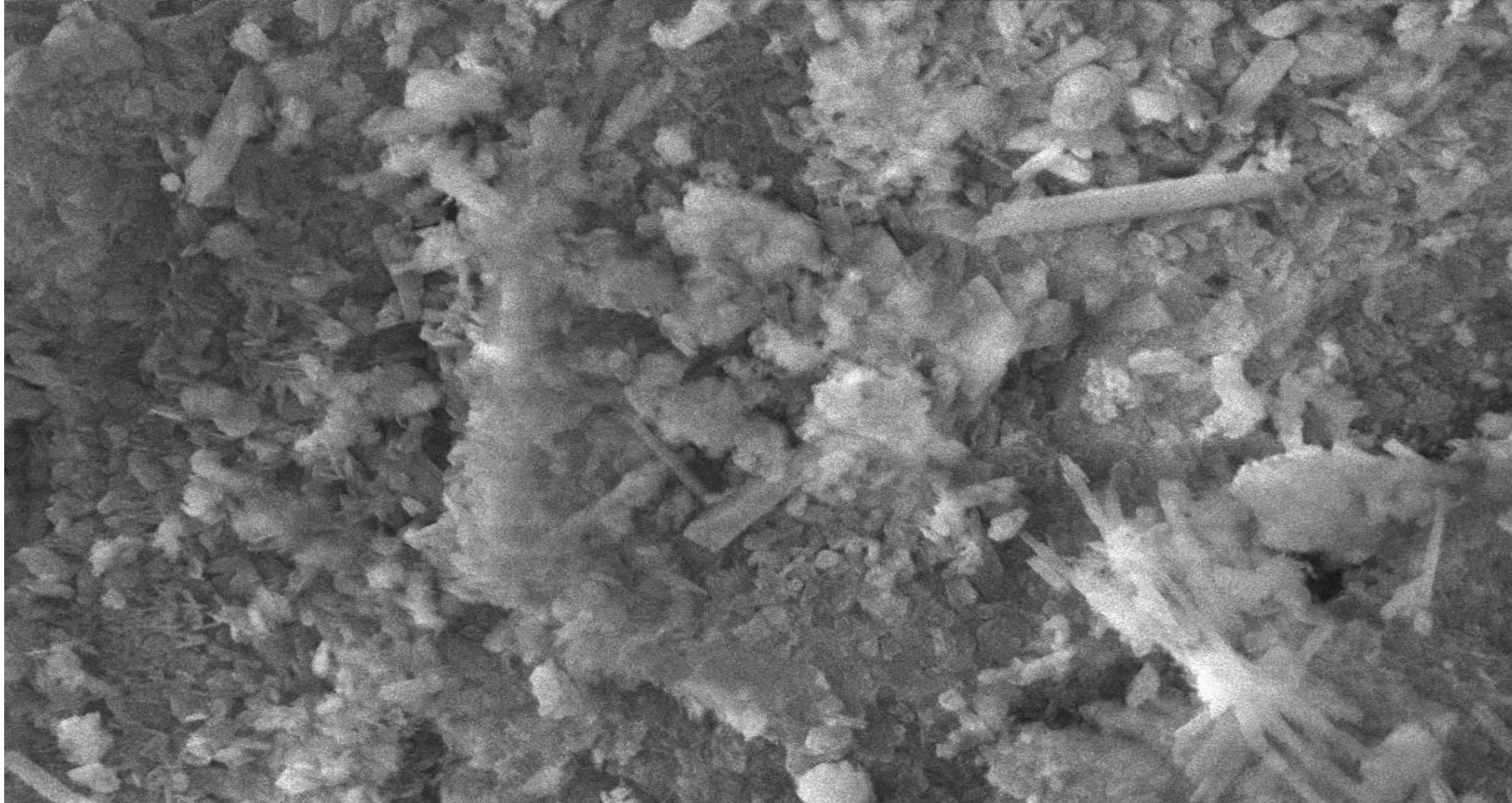
Signal A = SE1

WD = 7.5 mm

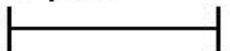
EHT = 20.00 kV

Mag = 10.00 K X Photo No. = 4911

View of sorbent partly saturated



1  $\mu$ m



EHT = 10.00 kV

WD = 7 mm

Signal A = InLens

Mag = 35.00 K X

Fresh sorbent



Different kind of filters used for biogas purification

# New generation filters



New ports in filters



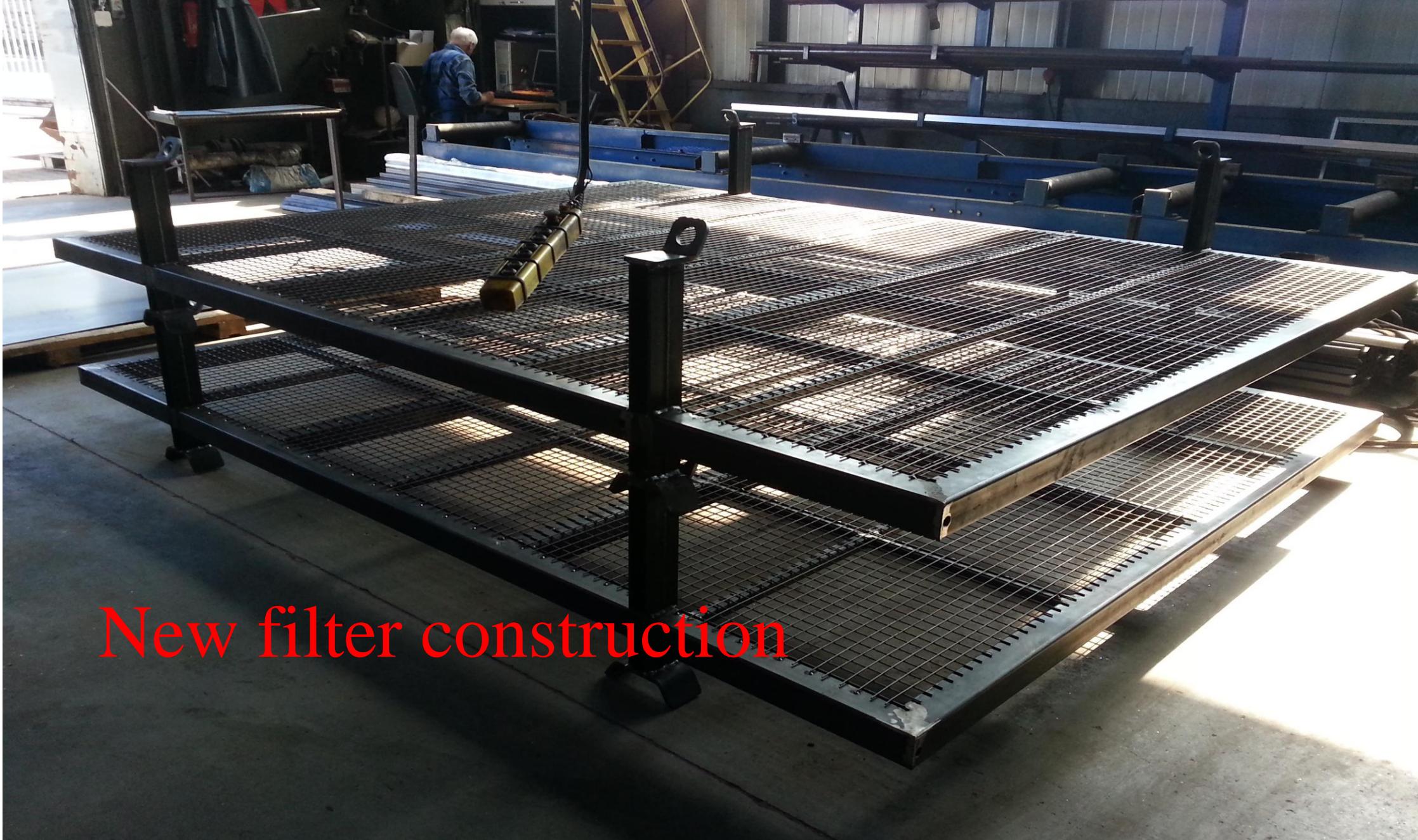
New ports for  
sampling



New equipment



New  
measurements



New filter construction

# Filter in Rybnik compost plant

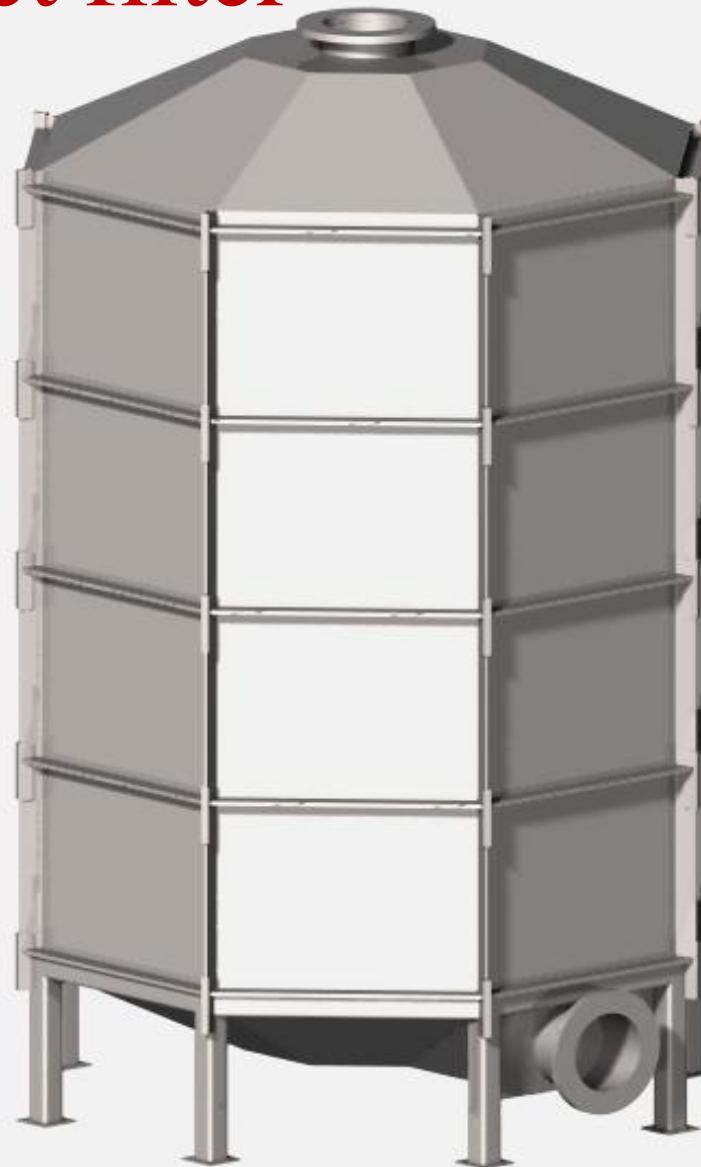


# Filter in Chorzów





# Compact filter



New compact biogas plant in  
Proboszczowice



**THANK YOU FOR YOUR ATTENTION**

